



DHLLDV Framework Graded Sands & Gravels

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Dredging A Way Of Life



Offshore A Way Of Life



What is Offshore & Dredging Engineering?

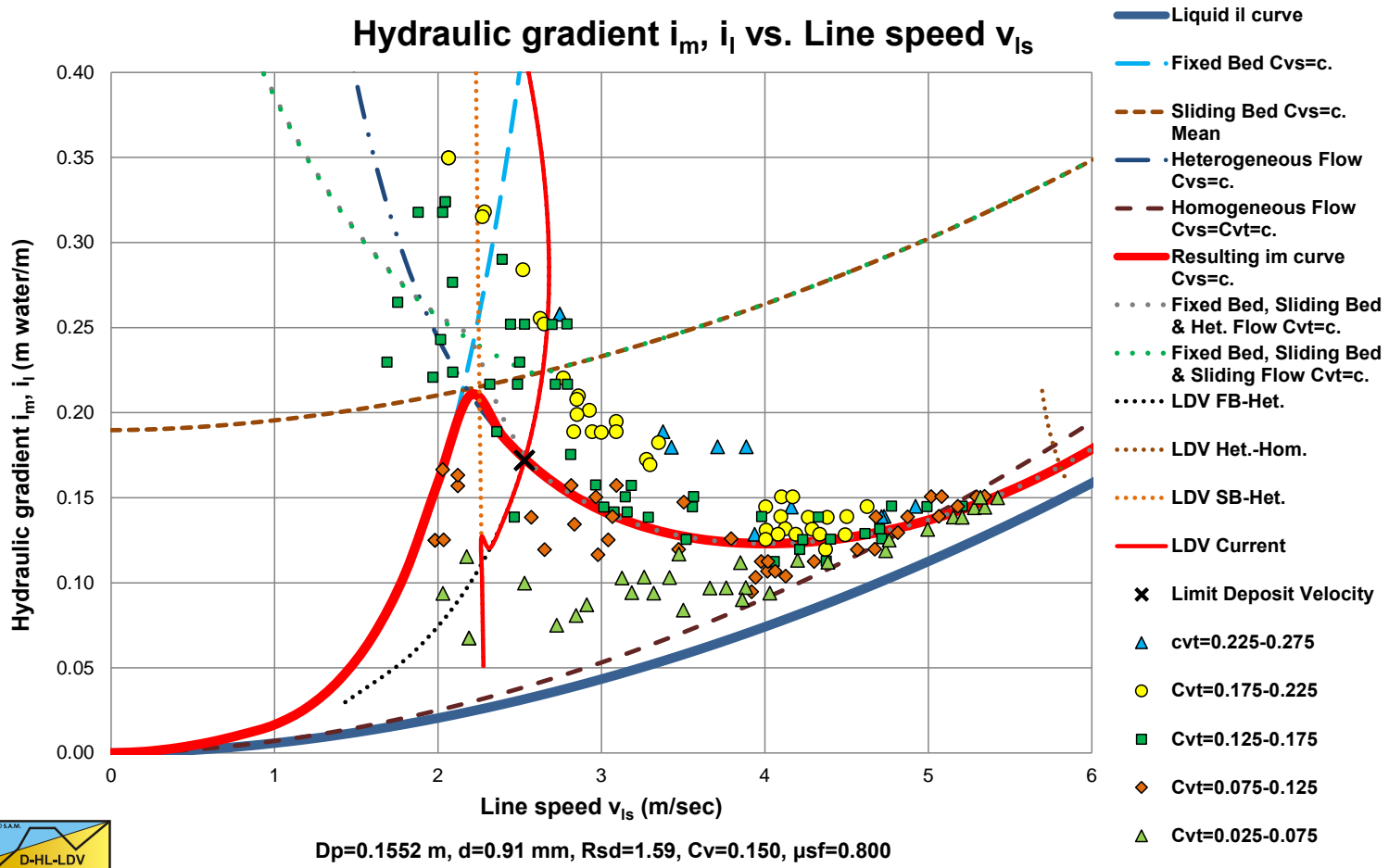
Offshore & Dredging Engineering covers everything at sea that does not have the purpose of transporting goods & people and no fishery.



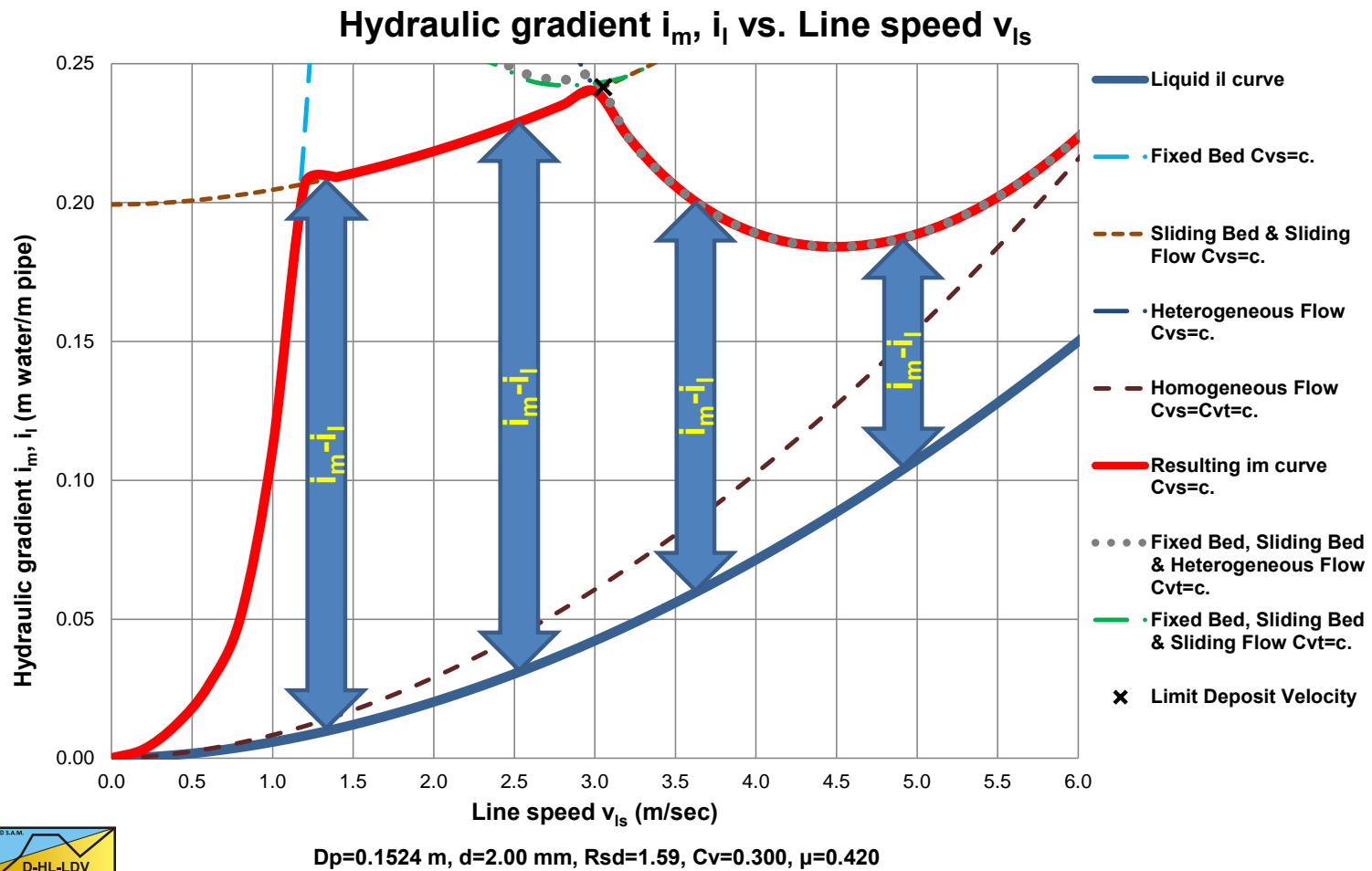


Introduction

Data from Yagi et al., C_{vs}



DHLLDV Model, The Solids Effect



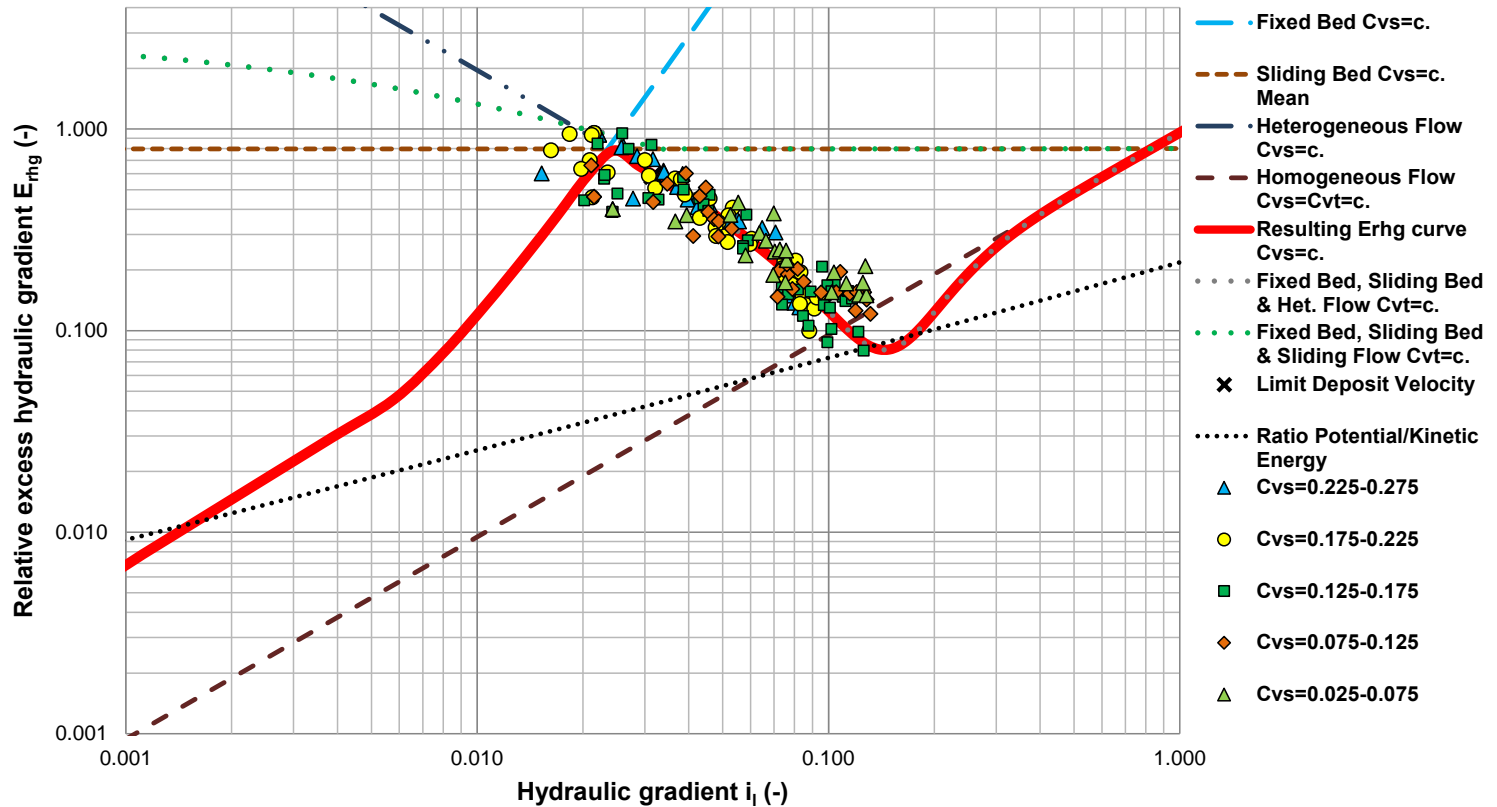
$$i_l = \frac{\Delta p_l}{\rho_l \cdot g \cdot \Delta L} = \frac{\lambda_l \cdot v_{ls}^2}{2 \cdot g \cdot D_p}$$

$$E_{rhg} = \frac{i_m - i_l}{R_{sd} \cdot C_v}$$

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Data from Yagi et al., C_{vs}

Relative excess hydraulic gradient E_{rhg} vs. Hydraulic gradient i_l



$D_p=0.1552$ m, $d=0.91$ mm, $R_{sd}=1.59$, $C_v=0.150$, $\mu_{sf}=0.800$



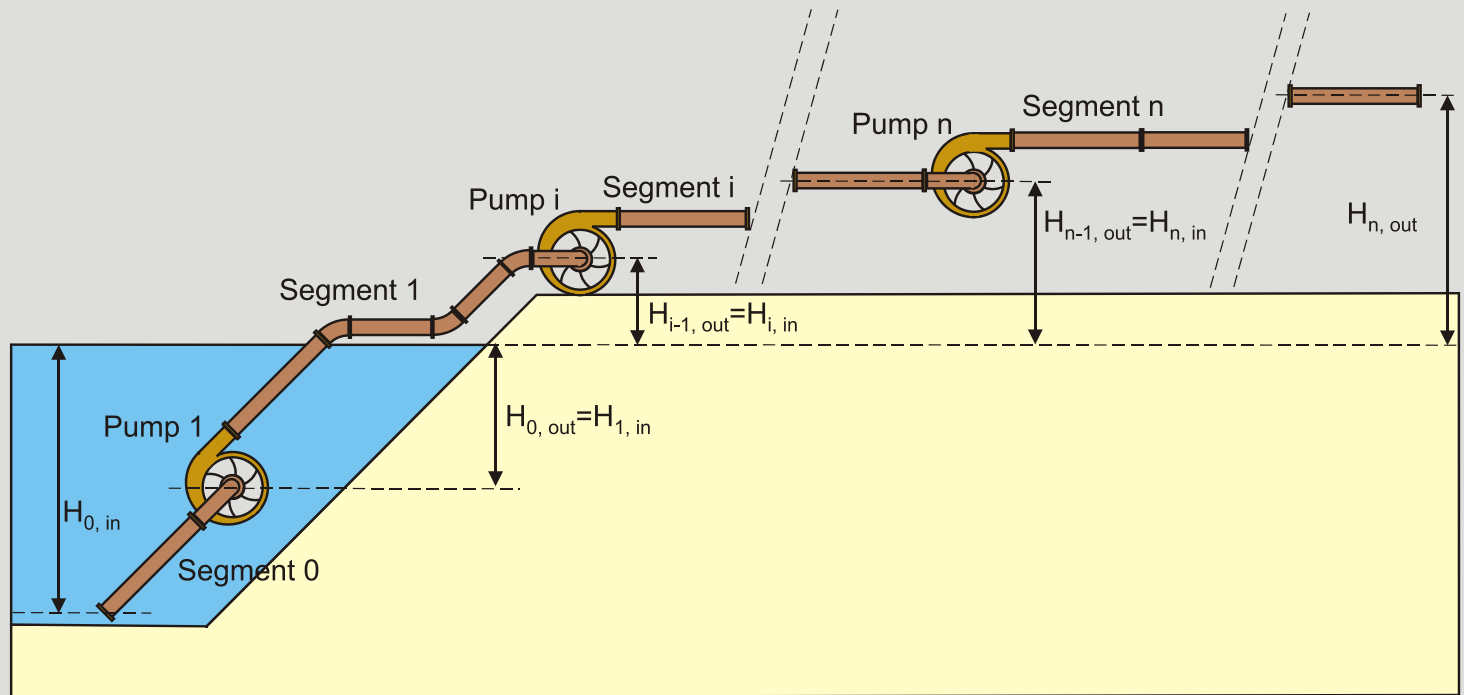


Inclined Pipes

Chapter 7.14 & 8.15



Pump/Pipeline System



- Total pressure/power required
- Cavitation limit of each pump
- Deposition/plugging the pipeline
- Limit Deposit Velocity



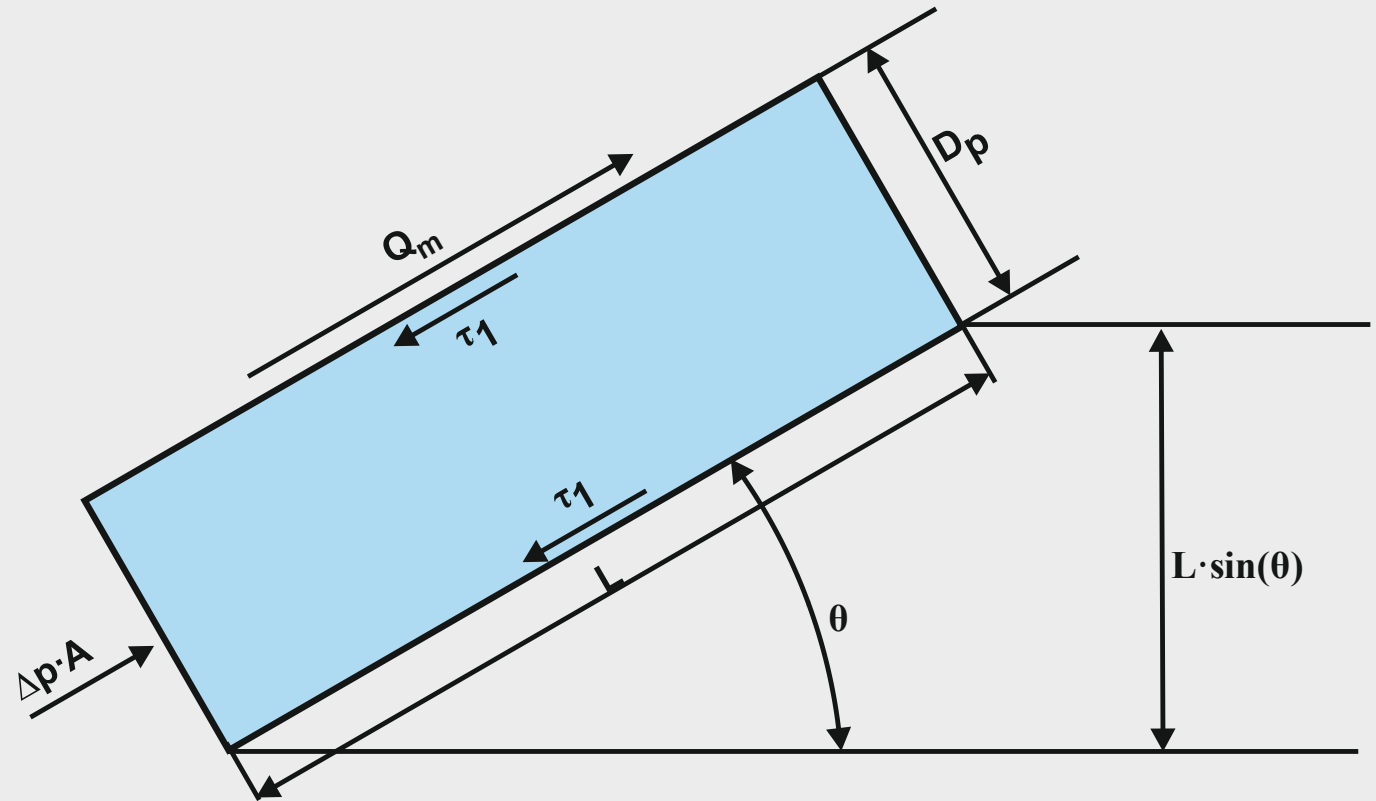
Research Question

Problem definition:

Existing methods for determining the hydraulic gradient (pressure losses) in inclined pipes simply multiply the hydraulic gradient of a horizontal pipe with the cosine of the inclination angle (to a certain power) and add the potential energy term. These methods do not consider the flow regimes.

- Flow regimes may respond differently to the inclination angle.
- The transition line speed between flow regimes may shift.
- Some flow regimes may not occur at all.
- The influence of the inclination angle has to be determined for each flow regime individually.

Pure Carrier Liquid



Pure Carrier Liquid

$$-\frac{dp}{dx} \cdot A \cdot L = \tau_1 \cdot O \cdot L + \rho_1 \cdot A \cdot L \cdot g \cdot \sin(\theta)$$

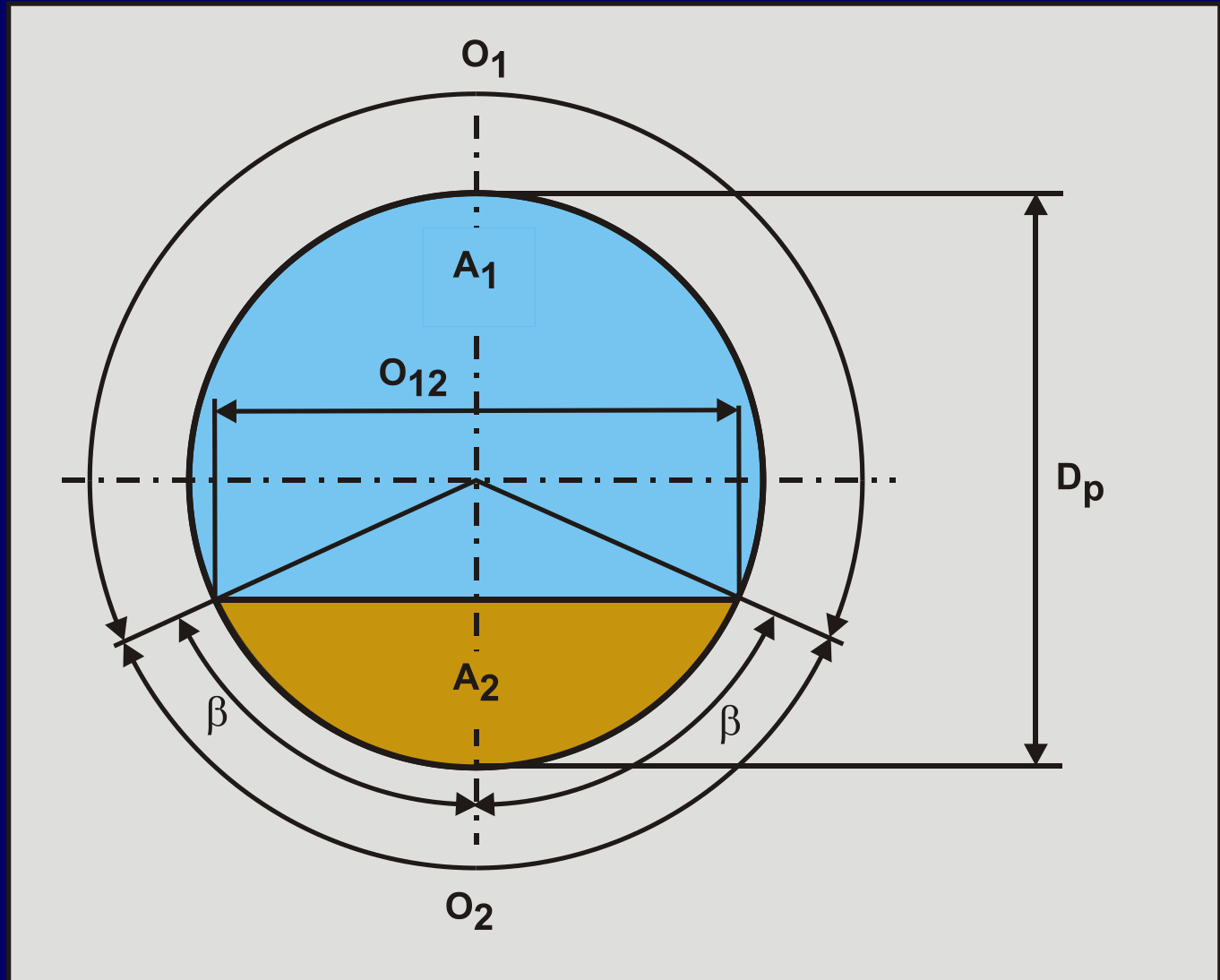
$$i_{1,\theta} = -\frac{dp}{dx} \cdot \frac{A \cdot L}{\rho_1 \cdot A \cdot L \cdot g}$$

$$= \frac{\tau_1 \cdot O \cdot L}{\rho_1 \cdot A \cdot L \cdot g} + \frac{\rho_1 \cdot A \cdot L \cdot g \cdot \sin(\theta)}{\rho_1 \cdot A \cdot L \cdot g}$$

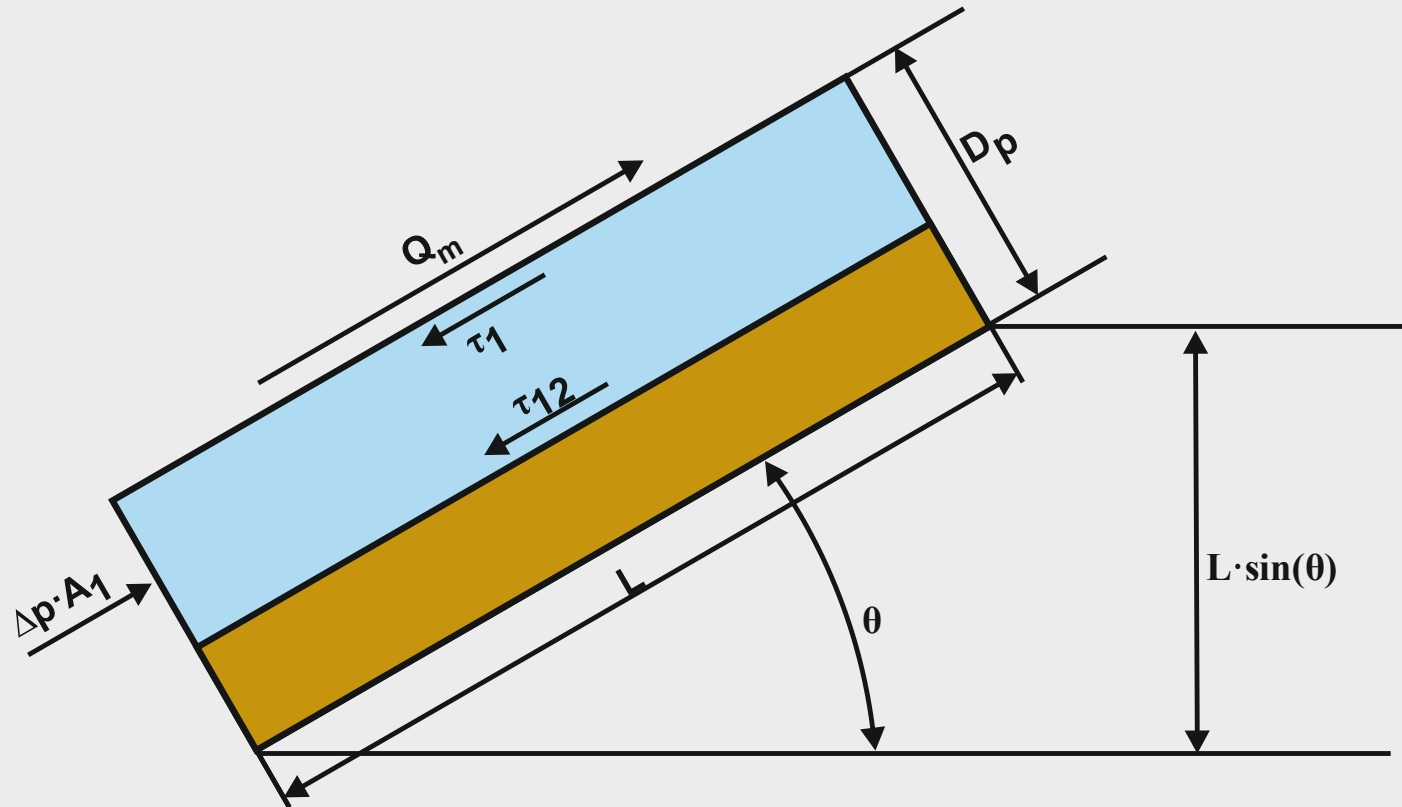
$$= i_1 + \sin(\theta)$$



Fixed/Sliding Bed Regime



Fixed/Sliding Bed Regime



Fixed Bed Regime

$$-\frac{dp}{dx} \cdot A_1 \cdot L = \tau_1 \cdot O_1 \cdot L + \tau_{12} \cdot O_{12} \cdot L + \rho_1 \cdot A_1 \cdot L \cdot g \cdot \sin(\theta)$$

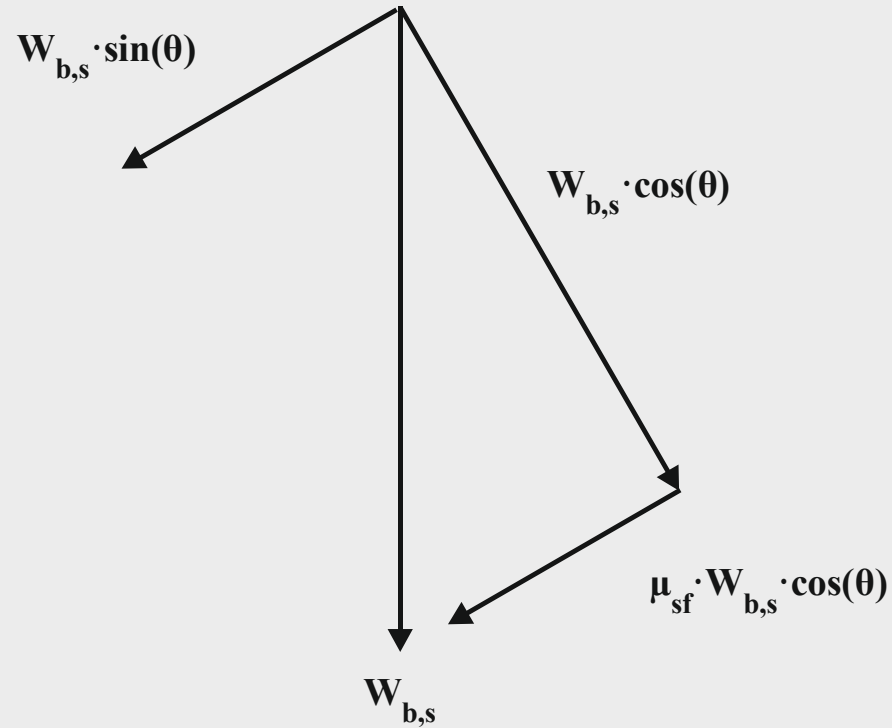
$$i_{m,\theta} = -\frac{dp}{dx} \cdot \frac{A_1 \cdot L}{\rho_1 \cdot A_1 \cdot L \cdot g}$$

$$= \frac{\tau_1 \cdot O_1 \cdot L}{\rho_1 \cdot A_1 \cdot L \cdot g} + \frac{\tau_{12} \cdot O_{12} \cdot L}{\rho_1 \cdot A_1 \cdot L \cdot g} + \frac{\rho_1 \cdot A_1 \cdot L \cdot g \cdot \sin(\theta)}{\rho_1 \cdot A_1 \cdot L \cdot g}$$

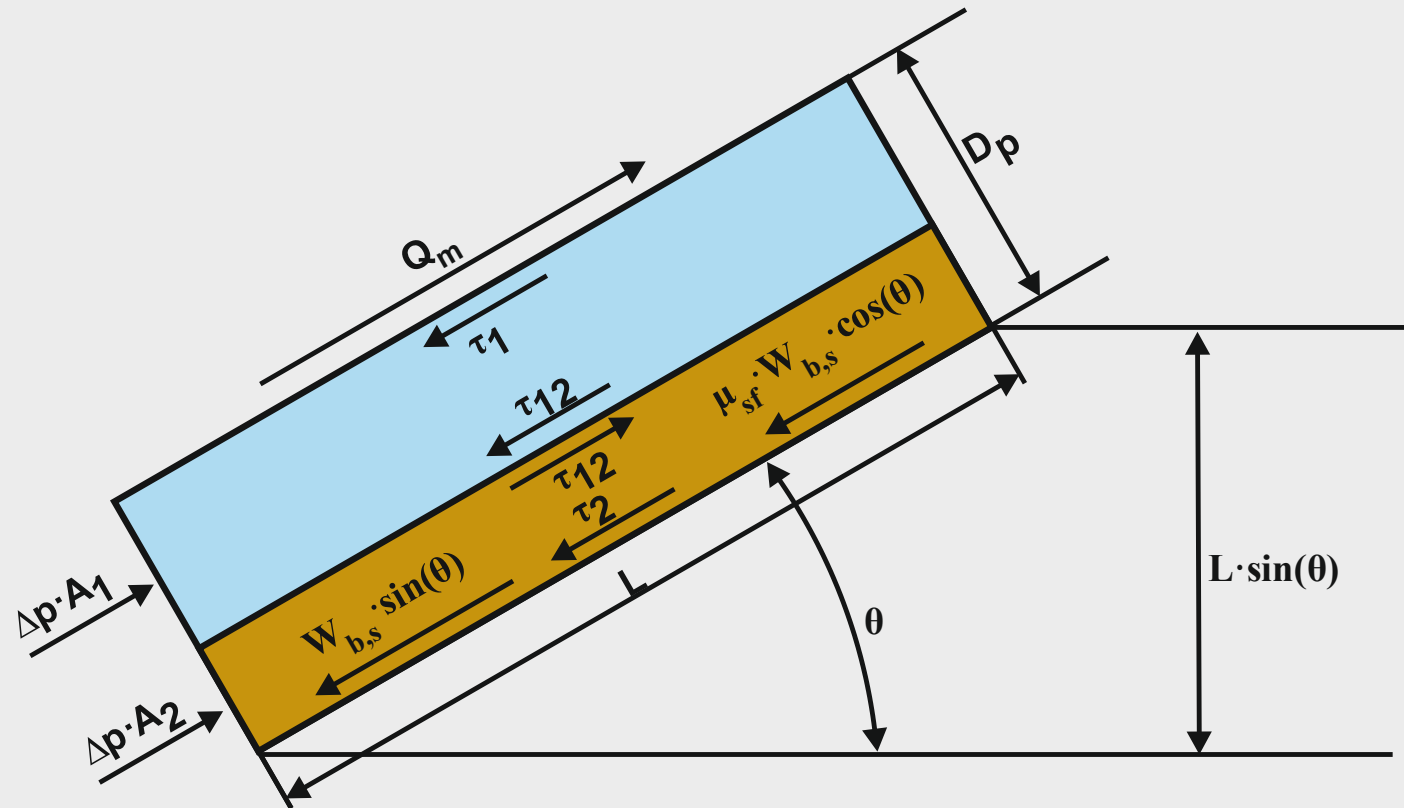
$$= i_m + \sin(\theta)$$



Sliding Bed Regime, Gravity



Sliding Bed Regime, Forces



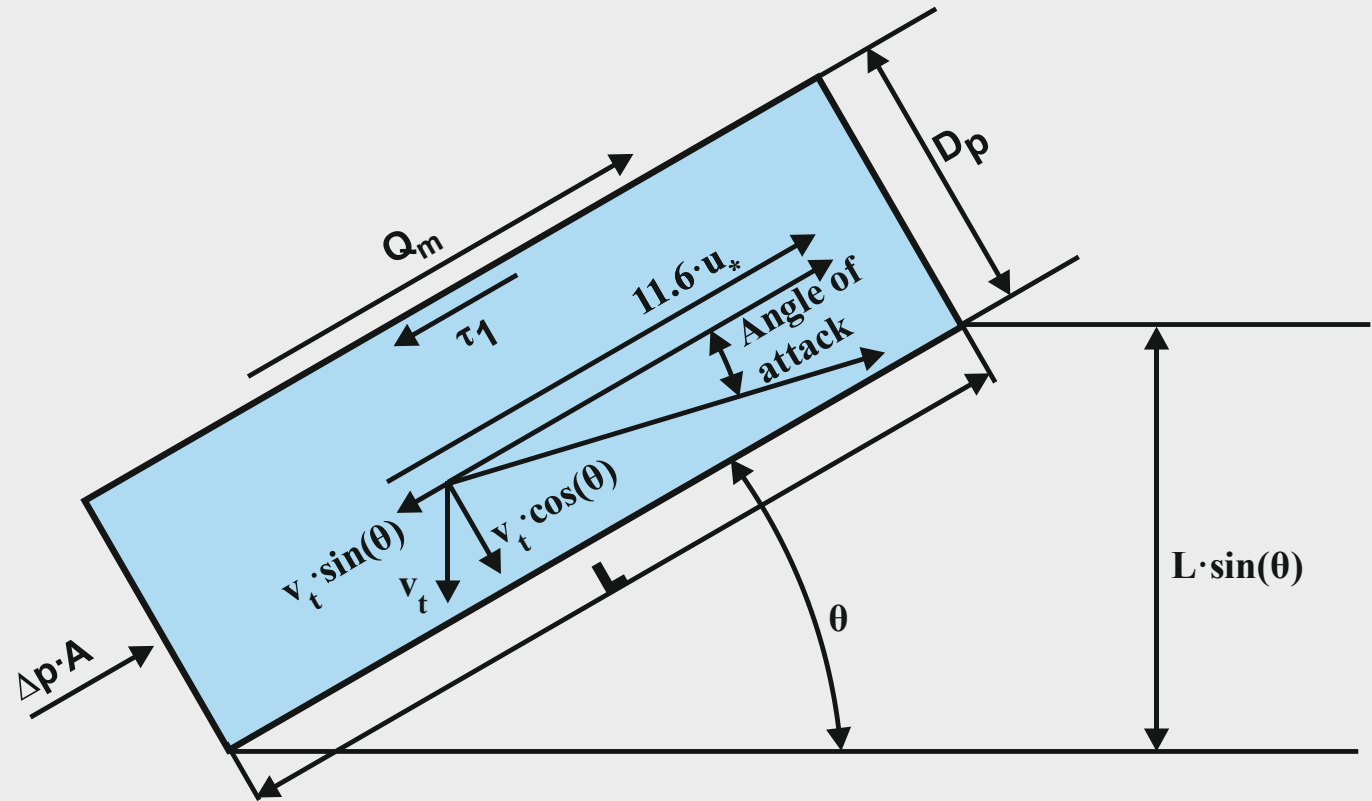
Sliding Bed Regime

$$i_{m,\theta} = i_{l,\theta} + R_{sd} \cdot C_{vs} \cdot (\mu_{sf} \cdot \cos(\theta) + \sin(\theta))$$

$$E_{rhg,\theta} = \frac{i_{m,\theta} - i_{l,\theta}}{R_{sd} \cdot C_{vs}} = \mu_{sf} \cdot \cos(\theta) + \sin(\theta)$$



Heterogeneous Flow Regime



Heterogeneous Flow Regime

$$S_{hr,\theta} = S_{hr} \cdot \cos(\theta) = \frac{v_t \cdot \cos(\theta) \cdot \left(1 - \frac{C_{vs}}{\kappa_C}\right)^\beta}{v_{ls}}$$

$$S_{rs,\theta} = c \cdot \left(\frac{\delta_v}{d}\right)^{2/3} \cdot \left(\frac{v_t \cdot \cos(\theta)}{11.6 \cdot u_* - v_t \cdot \sin(\theta)}\right)^{4/3} \cdot \left(\frac{v_t}{\sqrt{g \cdot d}}\right)^2$$

$$E_{rhg,\theta} = S_{hr,\theta} + S_{rs,\theta} + \sin(\theta)$$

$$i_{m,\theta} = i_{l,\theta} + \left(S_{hr,\theta} + S_{rs,\theta} + \sin(\theta)\right) \cdot R_{sd} \cdot C_{vs}$$



Homogeneous Flow Regime 1

$$i_{lm,\theta} = \frac{\lambda_1 \cdot (v_{ls} + v_{th} \cdot \sin(\theta) \cdot C_{vs})^2}{2 \cdot g \cdot D_p} + \sin(\theta)$$

$$\begin{aligned} i_{lm,\theta} &\approx i_1 + \sin(\theta) + i_1 \cdot \frac{2 \cdot v_{th} \cdot \sin(\theta) \cdot C_{vs}}{v_{ls}} \\ &= i_{1,\theta} + i_1 \cdot \frac{2 \cdot v_{th} \cdot \sin(\theta) \cdot C_{vs}}{v_{ls}} \end{aligned}$$

Homogeneous Regimes

$$i_{m,\theta} = i_1 \cdot (1 + \alpha_E \cdot R_{sd} \cdot C_{vs}) + (1 + R_{sd} \cdot C_{vs}) \cdot \sin(\theta)$$

Sliding Flow Regime

$$i_{m,\theta} = i_1 \cdot \left(1 + \frac{2 \cdot v_{th} \cdot \sin(\theta) \cdot C_{vs}}{v_{ls}} \right) + (1 + R_{sd} \cdot C_{vs}) \cdot \sin(\theta)$$



Homogeneous Flow Regime 2

Homogeneous Regimes

$$i_{m,\theta} = i_{l,\theta} + R_{sd} \cdot C_{vs} \cdot (\alpha_E \cdot i_1 + \sin(\theta))$$

Sliding Bed Regime

$$i_{m,\theta} = i_{l,\theta} + R_{sd} \cdot C_{vs} \cdot \sin(\theta) + i_1 \cdot \frac{2 \cdot v_{th} \cdot \sin(\theta) \cdot C_{vs}}{v_{ls}}$$

Homogeneous Regimes

$$E_{rhg,\theta} = \frac{i_{m,\theta} - i_{l,\theta}}{R_{sd} \cdot C_{vs}} = \alpha_E \cdot i_1 + \sin(\theta)$$

Sliding Bed Regime

$$E_{rhg,\theta} = \frac{i_{m,\theta} - i_{l,\theta}}{R_{sd} \cdot C_{vs}} = i_1 \cdot \frac{2 \cdot v_{th} \cdot \sin(\theta)}{v_{ls} \cdot R_{sd}} + \sin(\theta)$$

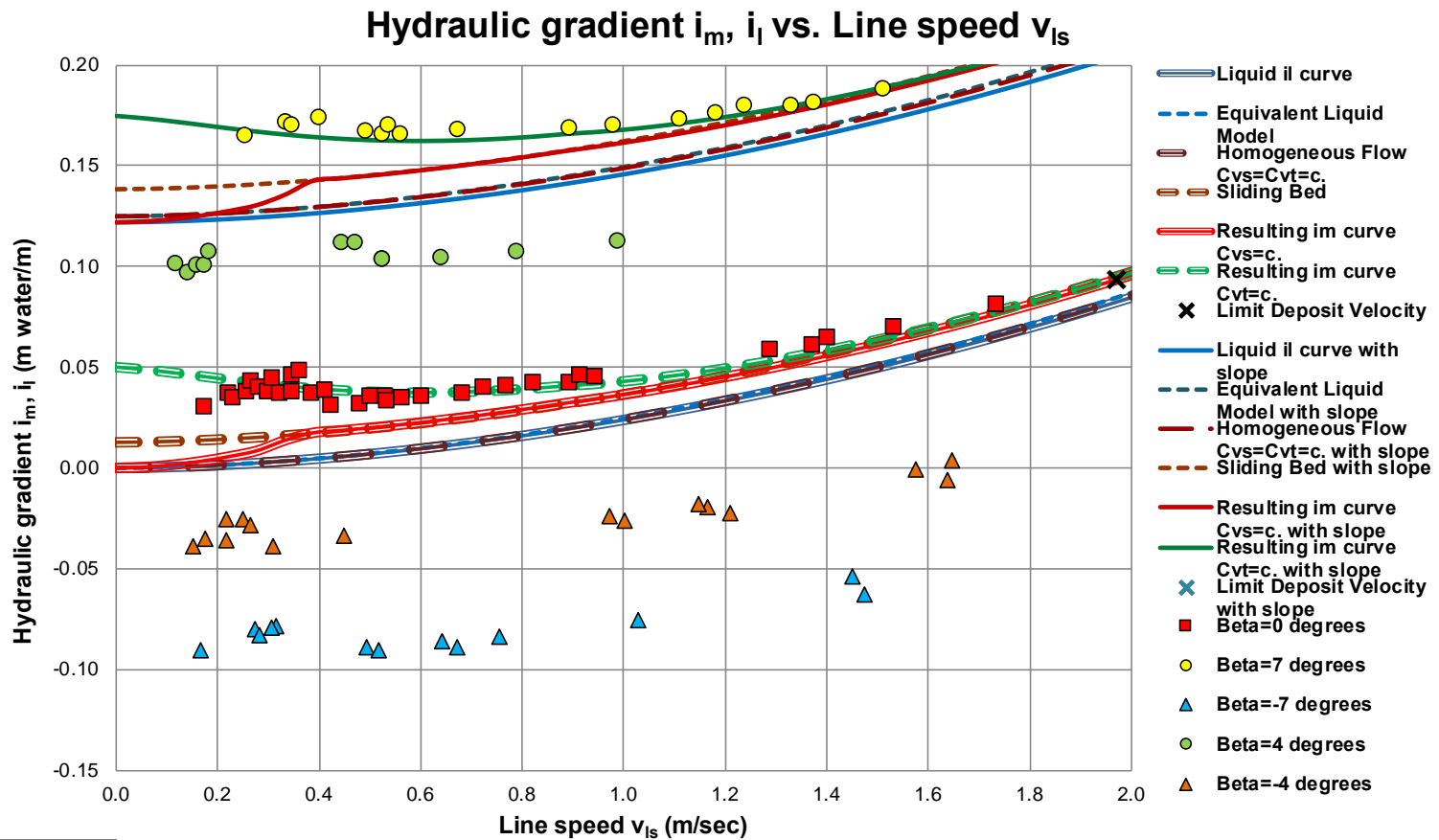


Limit Deposit Velocity

$$V_{ls,ldv,\theta} = V_{ls,ldv} \cdot \cos(\theta)^{1/3}$$



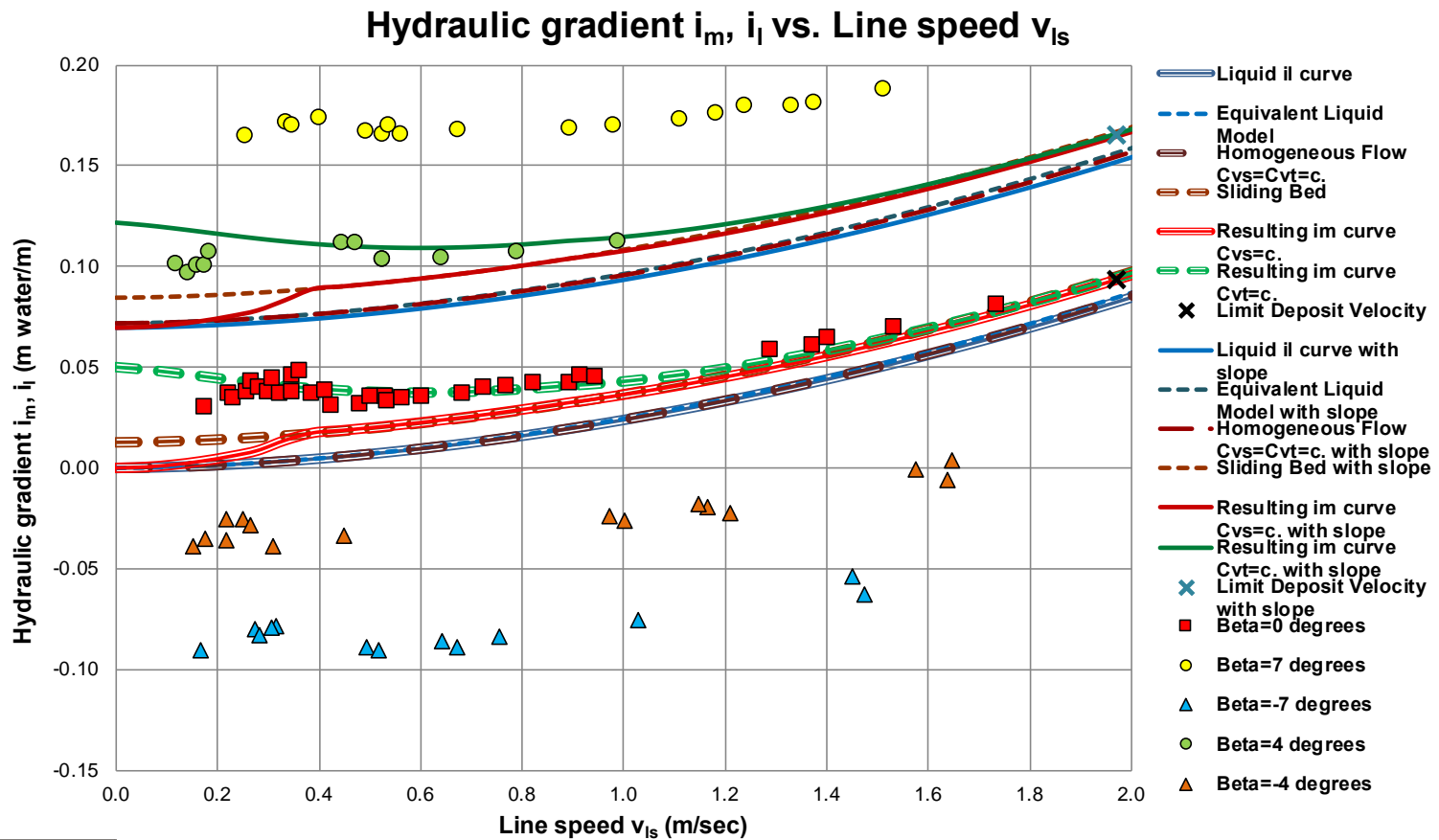
Inclined Pipe, Doron & Barnea (1997)



$D_p=0.0500$ m, $d=3.000$ mm, $R_{sd}=0.210$, $C_v=0.130$, $\mu_{sf}=0.480$, Slope= 7.0°



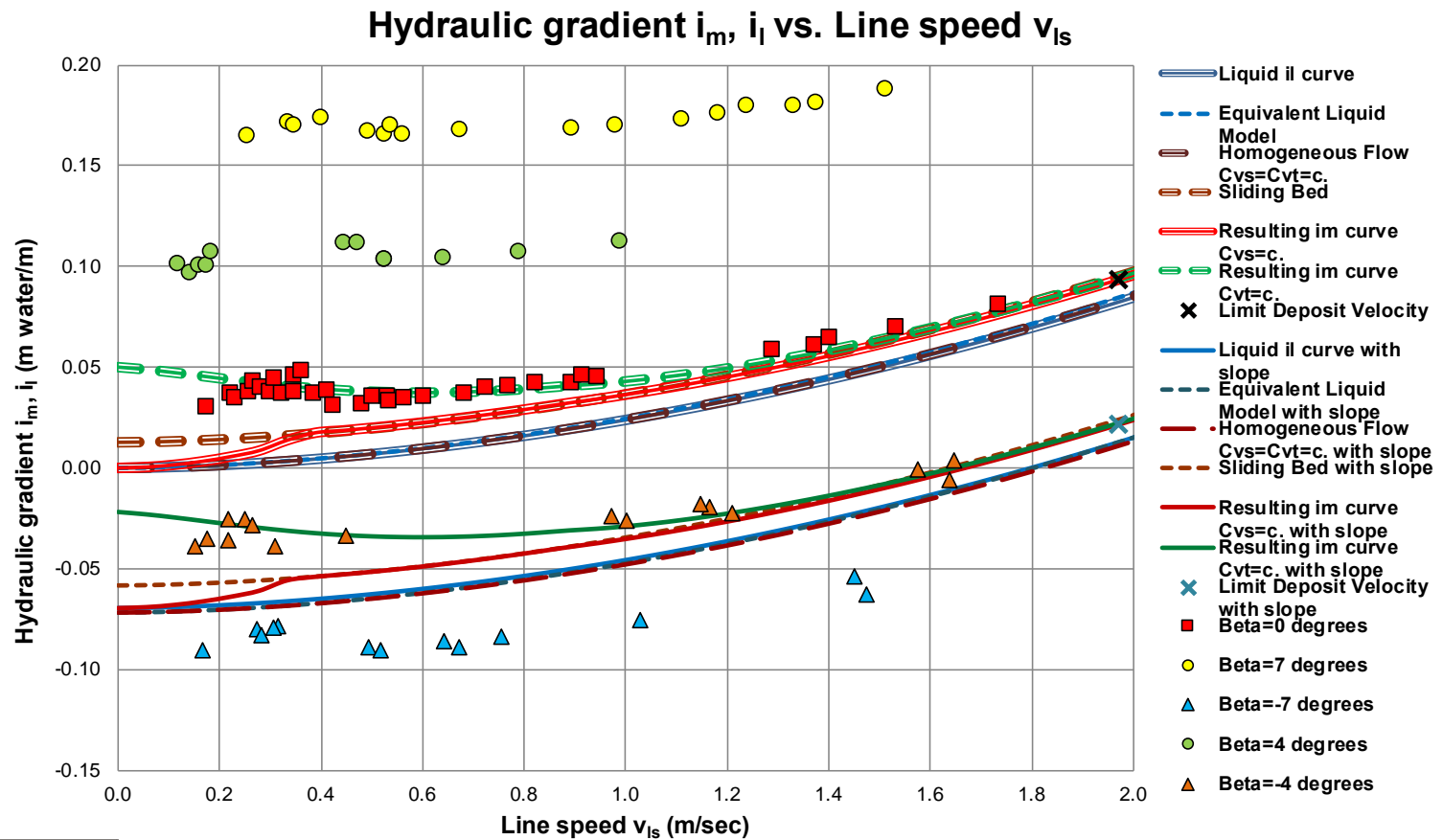
Inclined Pipe, Doron & Barnea (1997)



$D_p=0.0500$ m, $d=3.000$ mm, $Rsd=0.210$, $C_v=0.130$, $\mu_{sf}=0.480$, Slope= 4.0°



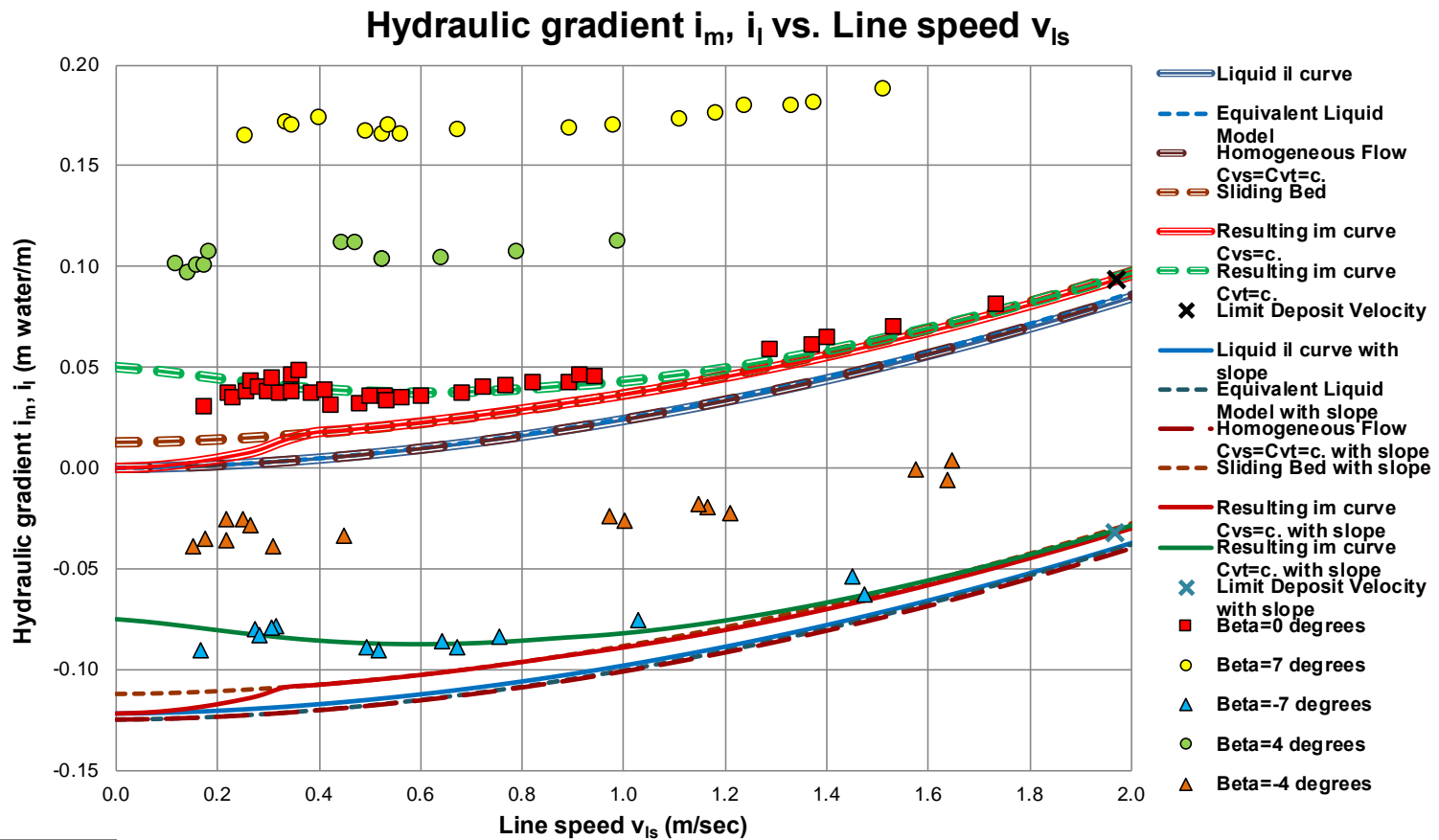
Inclined Pipe, Doron & Barnea (1997)



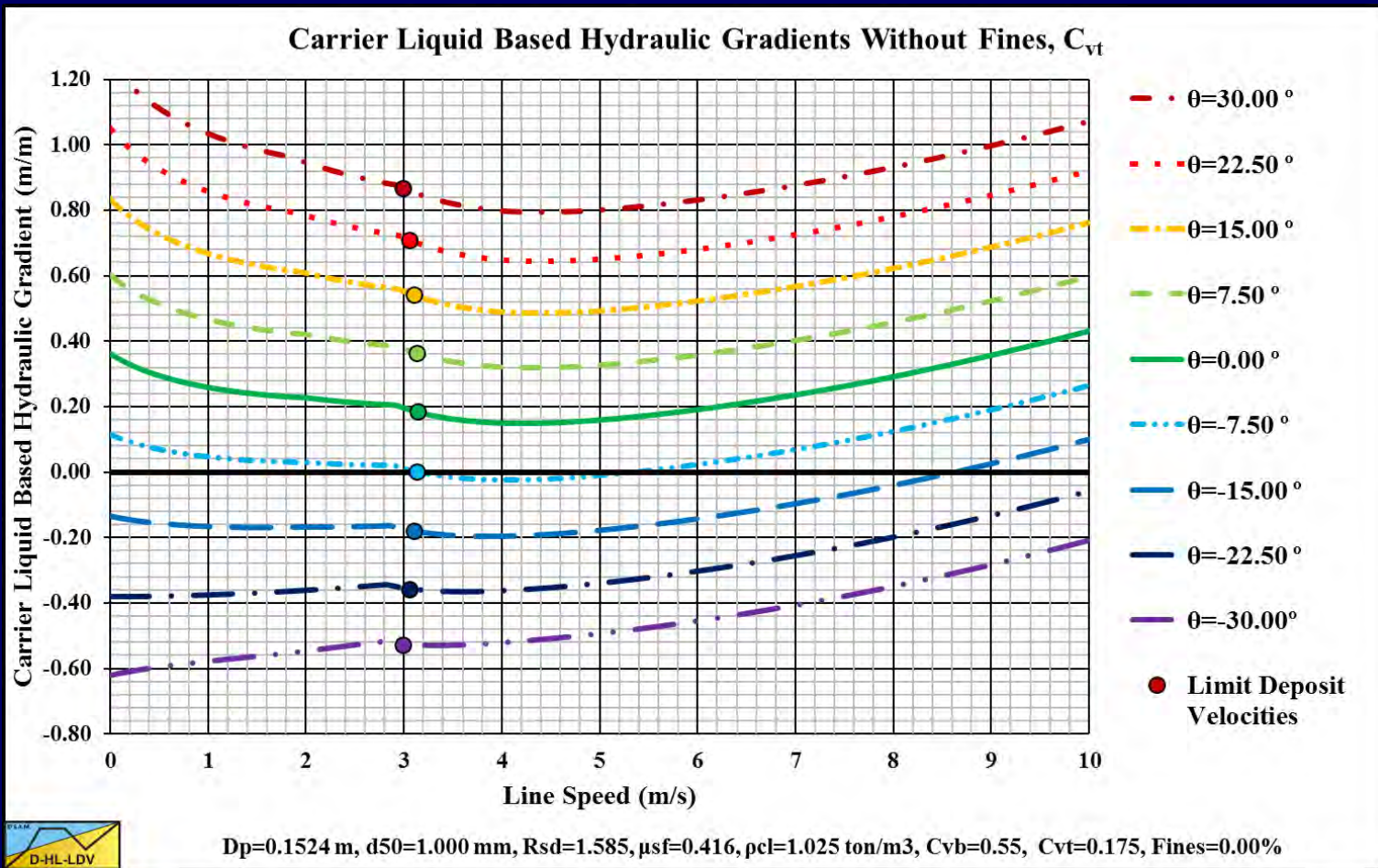
$D_p=0.0500$ m, $d=3.000$ mm, $R_{sd}=0.210$, $C_v=0.130$, $\mu_{sf}=0.480$, Slope= -4.0°



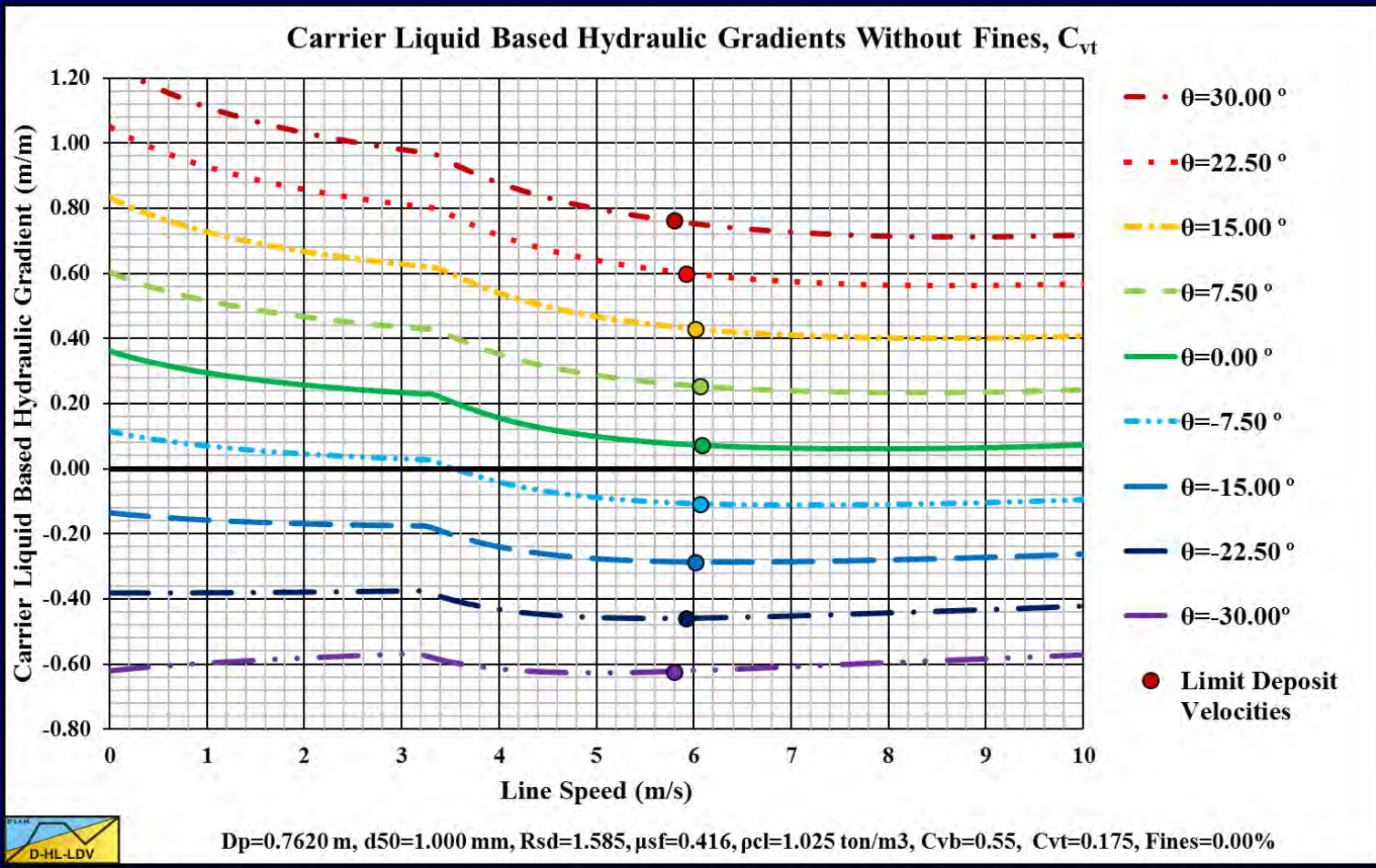
Inclined Pipe, Doron & Barnea (1997)



Inclined Pipe, $D_p=0.1524$ m, C_{vt}



Inclined Pipe, $D_p=0.762$ m, C_{vt}



Conclusions

- To construct the hydraulic gradient curve or relative solids effect curve for inclined pipes, first the curves for the different flow regimes have to be constructed.
- Secondly from the individual curves, a resulting curve can be constructed.
- The different flow regimes may behave differently with inclined pipes.
- The method described matches well with experimental data of Doron & Barnea, etc.





Questions?