# Two-Phase Modeling of Suspended Particle Flow



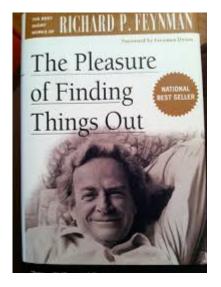


# **Dredging Engineering Group Delft**

"We believe that **knowledge** of dredging processes is the basis of a **competitive** and **sustainable** dredging industry which serves **mankind**"



# Why understanding?

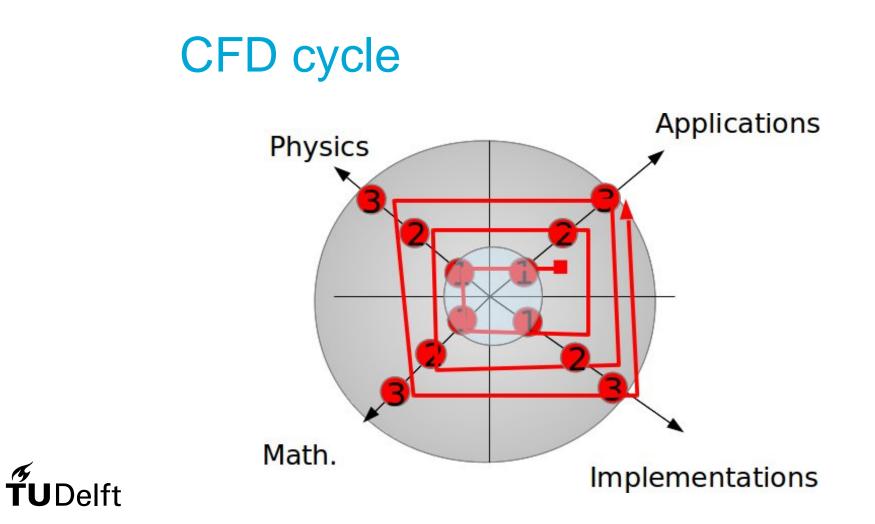




#### Research philosophy

# "Computational Fluid Dynamics is useful to acquire this knowledge"



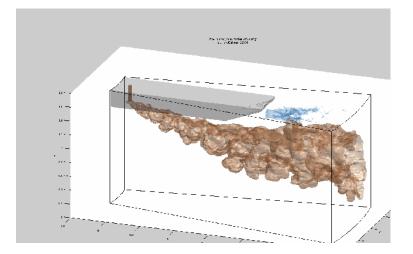


#### or in short

- Solve the right equations
  Solve them right
- 2) Solve them right



#### Example PhD project Lynyrd de Wit\*

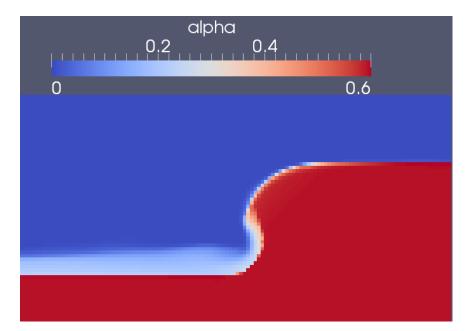


Overflow Plume of a TSHD

\*Present affiliation: Svasek Hydraulics



#### **Example 2 Dave Weij**



See his presentation on Thursday!



Unstable breaching / dilative slope failure ongoing work see his presentation!

# **Other PhD projects**

- Frans van Grunsven, deep-sea mining plumes (presentation 6:30 PM)
- Rudy Helmons rock cutting deep-sea mining (presentation Thursday)
- Bas Nieuwboer, mixture formation in a cutter
- Joep Goeree, generic mixture formulation.



#### **General approach**

#### Mixture approach involves super position

$$U_{particle} = U_{mix} + U_{settling} + U_{diffusion}$$

# See e.g. Goeree et al, 2016, The Canadian Journal of Chemical engineering



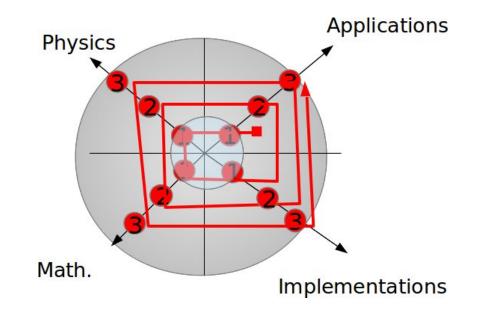
# Superposition of three velocities

- U<sub>mix</sub> Navier-Stokes equations for the mixture
- *U<sub>settling</sub>* settling test still water
- *U*<sub>diffusion</sub> passive scalar with many **corrections.**



# CFD Step 1

• Do we solve the right equations?





# Do we solve the right equations?

Near sand-water interfaces/rough walls?

- Velocity scales (V): friction velocity
- Length scales (L): distance to bed

Characteristic time-scales (L/V) versus particle response times?



# **Original two-phase equations**

- Momentum equation for water
- Momentum equation for solid
- Indicator function to detect presence of each phase
- Coupling forces between the solid and water velocity fields



Analysis of relevant scales in equilibrium channel flow problem

- Basic equations Drew (1975)
- Re-analysis and closures of Greimann et al, (1999) and (2001)
- Re-analysis Keetels et al (2016)

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#### Re-analysis by Keetels et al, 2016\*

Relevant local scaling group based on

- Particle response time
- RMS solid velocity field fluctuations
- Turbulent diffusion coefficient

\*Under review at Journal of Hydraulic Research



#### Result

- Inertia terms in the solid momentum equations can not be neglected near the wall!
- For coarse particles with large response times these terms are even more important!
- Fine particles sufficiently far from wall safe to use mixture approach



#### **Fine particles**

- Neglecting inertia terms in two-phase framework results in traditional profiles (Rouse 1937, Hunt 1954, Hallbron 1949)
- Generalization of Greimann et al, (2001) with respect to non-linear drag and hindered-settling (particle crowding effect)



# **Coarse particles**

- Essential to model the inertia terms in the momentum equation of the solid phase
- Greimann, 2001 uncertainty in two-key parameters
- Coupling fluid and solid velocity fluctuations?
- Coefficient of restitution of particles in viscous flow?



#### Coupling fluctuations solid and fluid

 Ct model of Issa and correction of Behzadi et al, (2004).

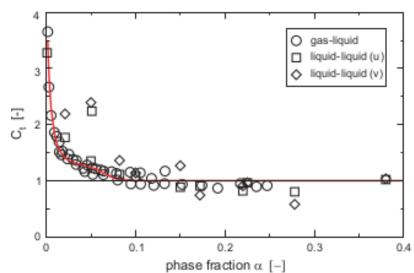




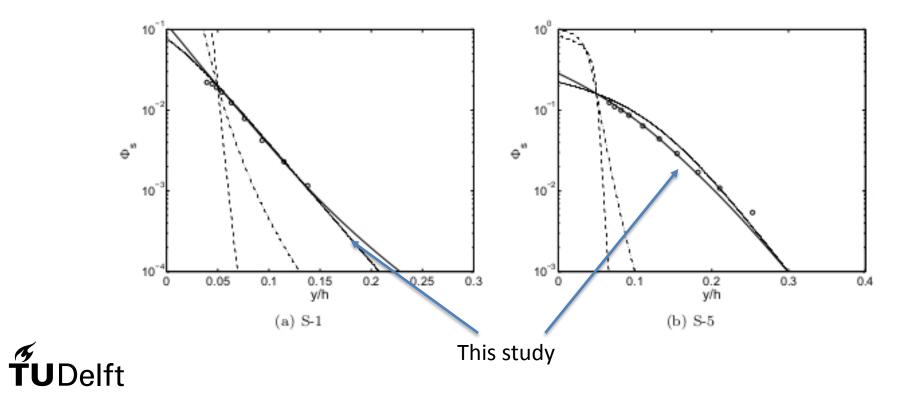
Fig. 3. Turbulence response function as a function of the phase fraction.

# **Restitution coefficient**

- Experiments of Anguilar-Corona et al (2011)
- Correction of dry restitution coefficient as a function of a Stokes number alike parameter.
- Greimann 2001, used dry value because information in viscous flow was not available.



#### **Concentration profiles**



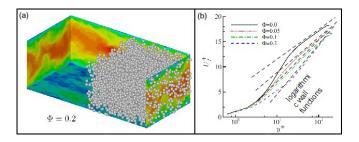
### Conclusion

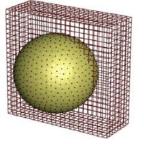
- Fine particle sufficiently far from wall safe to use mixture approach (super position of hindered-settling and diffusion)
- Coarse particle require two-phase approach
- With realistic closures reasonable accurate prediction of concentration profiles.



#### Next step

- More advanced modelling to predict both velocity and concentration profile, see also Goeree et al, 2016.
- Lack of information, Direct Numerical Simulation on particle level (Wim-Paul Breugem).







#### Insert a picture



# Insert a picture



